



Industrial Application of Anaerobic Digestion Technology

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Presentation Outline

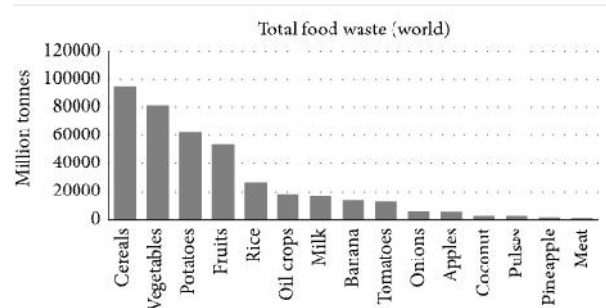
- Introduction
- Benefits of anaerobic digestion
- Reaction details
- Process value chain
- Economic relevance
- Factors affecting rate of anaerobic digestion (AD)
- AD design parameters and process configurations
- Deployment of AD for industrial application

Introduction

- Global food waste contribution to env. pollution (Paritosh et al., 2017)

- Industrial organic waste contributors

- food and beverage industry
- pulp and mill industry
- agricultural industry
- agro-allied industry
- petrochemical industry
- leather industry
- tannery industry



Introduction (Cont'd)

- Techniques for Management of organic wastes

- Composting
- Recycling
- Aerobic digestion
- Anaerobic digestion

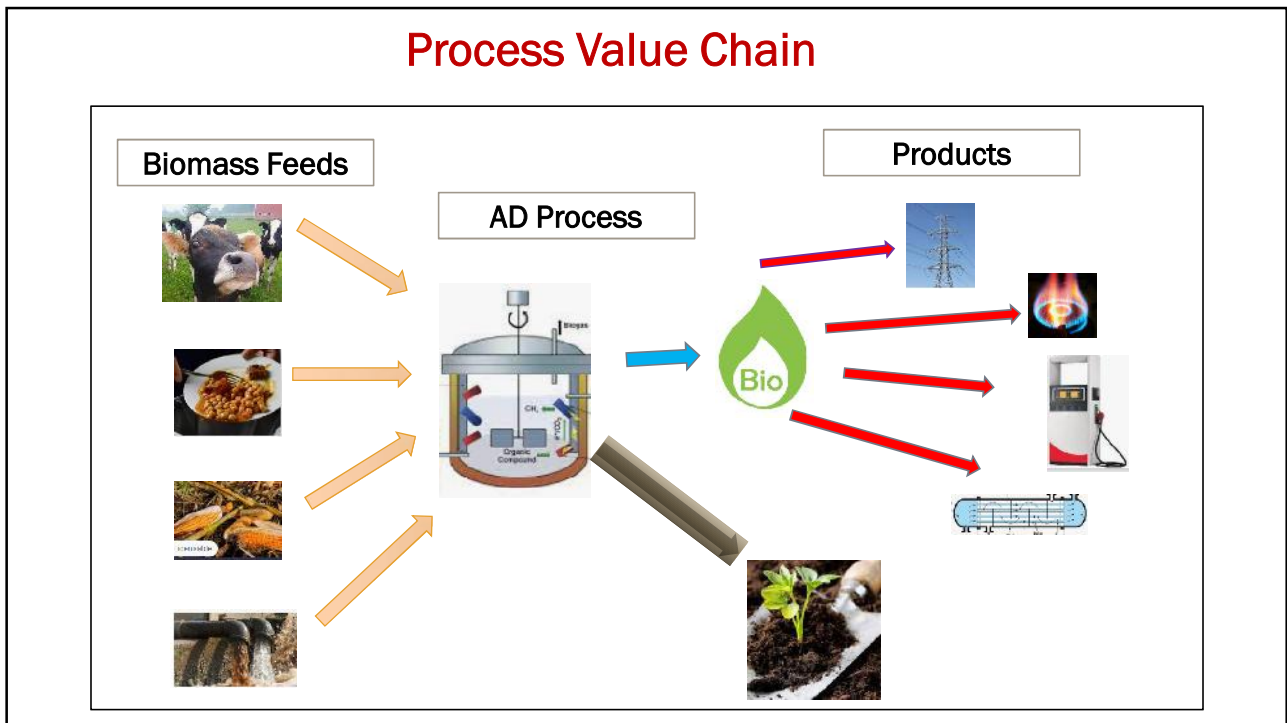
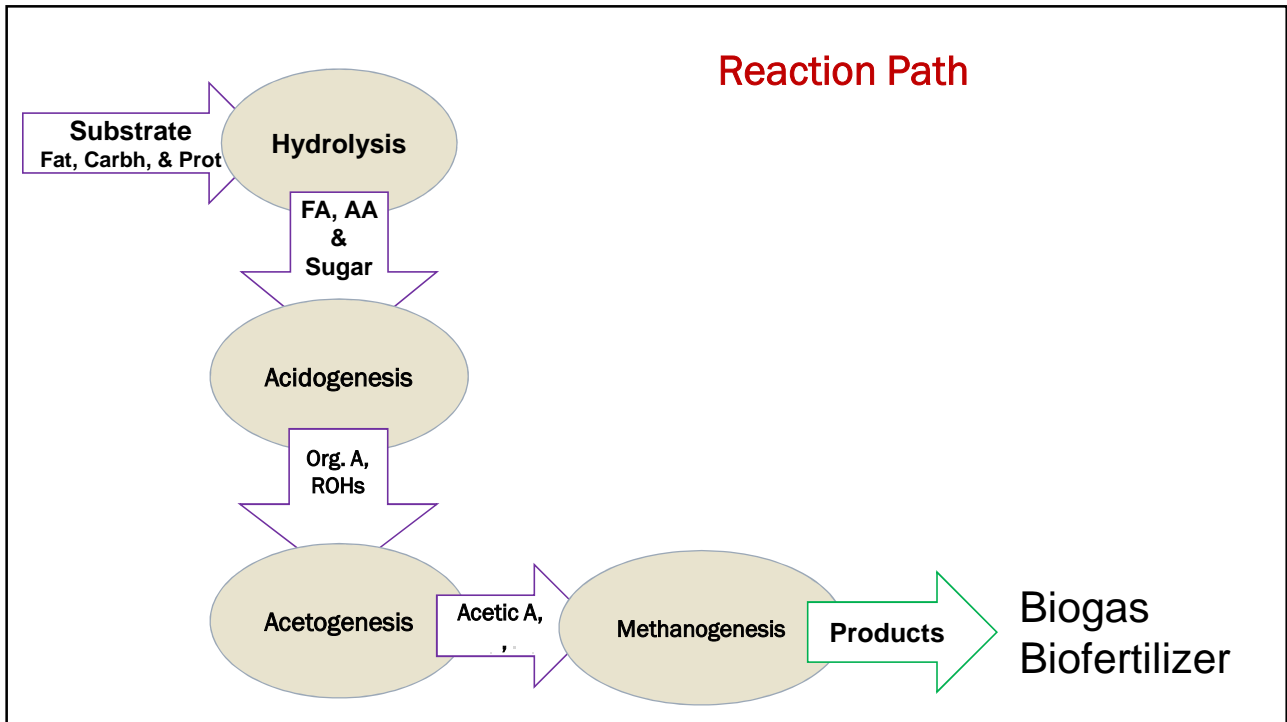
- Anaerobic Digestion (AD): It is a biochemical process involving the breakdown of organic wastes into simpler molecules by the microbial activities of microorganism

Benefits of Anaerobic Digestion

- Purely a biological process hence it's environmentally friendly
- Reduces release of air and water pollutant into the environment
- Removes harmful pathogens from biological waste
- Reduces carbon footprint thereby serving as potent mitigation against climate change
- Converts waste to wealth
- Low operating costs
- Proven effectiveness

Reaction Details

- The reaction proceeds via a four-stage mechanism
 - hydrolysis,
 - acidogenesis,
 - acetogenesis
 - methanogenesis
- Products of anaerobic digestion
 - biogas (50% – 75% CH_4)
 - carbon dioxide
 - Nitrogen gas
 - hydrogen sulfide
 - water vapour
 - biofertilizer
 - traces of other gas such as hydrogen



Global Relevance and Economic Potentials

- AD has been adopted worldwide, ranging from small-scale household digesters to large-scale systems
- Globally Europe is leading in AD technology deployment their leading role is mainly driven by strict environmental regulations for waste disposal
- Zaks et al., 2011 reported that AD systems in USA have the potential to generate 5.5% of USA annual electricity generation
 - This is equivalent to about 231 TWh
 - At energy cost of 10.42 cent/kWh; this is worth \$104 billion/annum

Factors Affecting Rate of Anaerobic Digestion

- Absence of oxygen
- Dynamic of microbial population
- pH; best at 6.8 – 7.2
- Reaction temperature
 - Psychrophilic; 10 – 20°C
 - Mesophilic; 20 – 48°C
 - Thermophilic; > 48°C

AD Design Parameters and Process Configurations

- Selection of process configuration
 - Reactor type
 - Batch reactor
 - Sequencing Batch [anaerobic sequencing batch reactor (ASBR)]
 - Continuous reactor; continuous stirred tank reactor (CSTR)
 - Semi-Continuous reactor
 - Reaction kinetic rate order
 - 1st order
 - 2nd order
 - Fractional order
 - Reaction rate constant (k)
 - Overall rate constant is determined or adopted
 - Reaction stages
 - single stage or multiple stage

Reactor Design Equations

- For a reaction involving reactant A, rate of consumption of A is;

$$-r_A = k C_A^n \quad (i)$$

Where k = the rate constant which is dependent on the reaction temperature and the activation energy

C_A = concentration of A at any given time t , after commencement of the reaction

n = kinetic rate order of the reaction

- **1st order batch reactor (using MTR)**

$$t = \int_{C_A}^{C_{A0}} \frac{C_A}{k C_A} = - \int_{C_A}^{C_{A0}} \frac{1}{k} \quad (ii)$$

- For 1st order kinetics; $t = - \int_{C_A}^{C_{A0}} \frac{1}{k} = - \ln\left(\frac{C_A}{C_{A0}}\right) \quad (iii)$

$$\text{But, } t = - \ln\left(\frac{C_A}{C_{A0}}\right) \quad (iv)$$

$$\text{Therefore, } V = - \ln\left(\frac{C_A}{C_{A0}}\right) = - \ln\left(\frac{C_A}{C_{A0}}\right) \quad (v)$$

- **1st order continuous/semi-continuous reactor (using CSTR)**

- $V = \frac{F_A (1 - X)}{k X}$ (vi)

- For 1st order kinetics; $V = \frac{F_A (1 - X)}{k X}$ (vii)

- But, $X = 1 - \frac{F_A}{F_A + k V}$ (viii)

- Also, $X = \frac{k V}{F_A + k V}$ (ix)

- Therefore, $V = \frac{(F_A + k V)}{k X} = \frac{(F_A + k V)}{k}$ (x)

2nd Order Kinetic Design Equations

- **Batch reactor (using MTR)**

- $V = - \left(\frac{F_A}{k} \left(\frac{1}{X} - \frac{1}{X_0} \right) \right) = \frac{(F_A)}{k X}$ (xi)

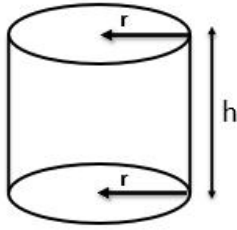
- Therefore, $V = \frac{(F_A)}{k X}$ (xii)

- **Continuous or semi-continuous reactor (using CSTR)**

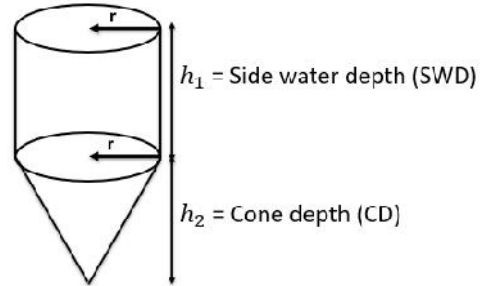
- $V = \frac{F_A (1 - X)}{k X^2} = \frac{(F_A)}{k X}$ (xiii)

- Therefore, $V = \frac{(F_A)}{k X}$ (xvi)

Sizing of Reactor



Or



- $d = \sqrt{\frac{V}{\pi h}}$ (xv)

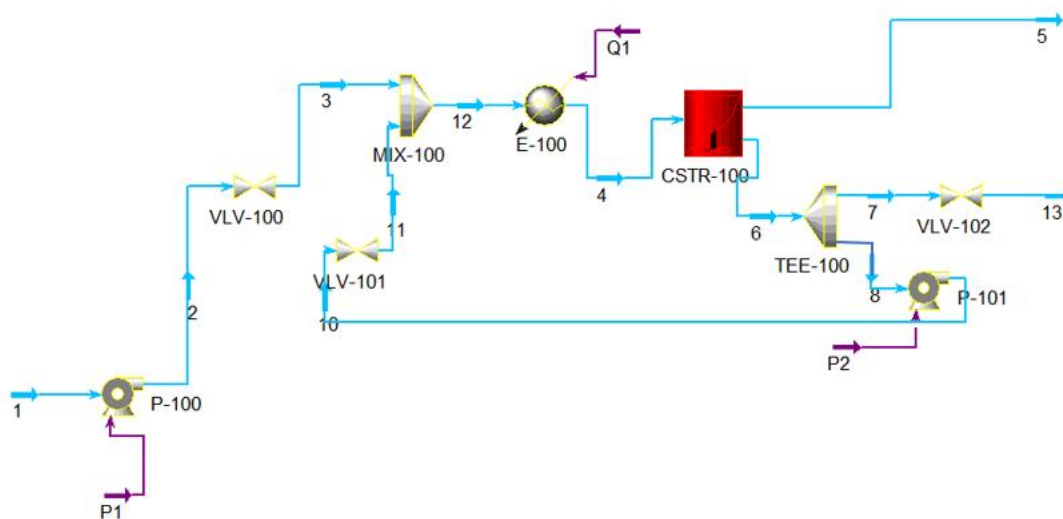
- $h = \frac{V}{\pi d^2}$ (xvi)

- $d = \sqrt{\frac{V}{\pi h_1}}$ (xvii)

- $h = \frac{V}{\pi d^2} + \frac{3}{4} \frac{V}{\pi d^2} \frac{h_2}{h_1}$ (xviii)

- $h = \frac{V}{\pi d^2} + \frac{3}{4} \frac{V}{\pi d^2} \frac{h_2}{h_1}$ (xix)

Typical Process Flow Diagram of An AD System



Stage by Stage Steps for Deployment of AD for Industrial Application

- Determining design parameters
- Design of the digester (reactor)
- Design of the auxiliary unit operations such as;
 - pumps
 - mixer
 - heat exchanger etc
- Generation of process flow diagram (PFD) using computer simulation;
 - Hysys
 - Aspen plus
- Fabrication of the various unit operations
- Installation
- Commissioning of the AD plant



